

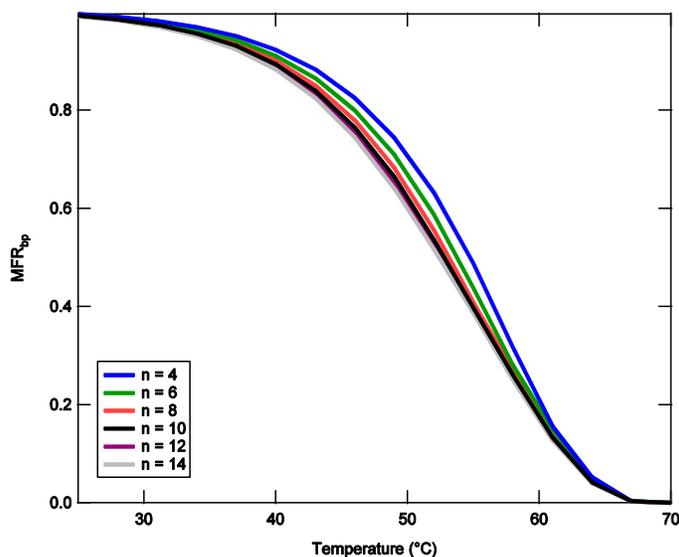
## Supplementary Material for “A model of aerosol evaporation kinetics in a thermodenuder” by C. D. Cappa<sup>1</sup>

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### Influence of the number of bins

The TD model described in the main text requires the user to specify some number of bins,  $n$ , that defines the number of concentric cylinders that the system is divided into. A choice of  $n = 10$  provides a reasonable tradeoff between overall accuracy and computational speed. Only very small changes are found in the calculated mass fraction remaining (MFR) values for  $n > 10$ . However, when smaller values of  $n$  are used the calculated MFR is greater at a given temperature, indicating less overall evaporation occurred. Results are shown in Figure S1 for calculations performed using  $C_{sat} = 1 \mu\text{g}/\text{m}^3$ ,  $C_{OA} = 10 \mu\text{g}/\text{m}^3$ ,  $\Delta H_{vap} = 120 \text{ kJ}/\text{mol}$ ,  $d_p = 200 \text{ nm}$ ,  $D_i = 3 \times 10^{-6} \text{ m}^2/\text{s}$ ,  $t_{res} = 15 \text{ seconds}$  and the adsorbent denuder boundary condition (Case 1 in the main text). Only very small differences in the calculated  $MFR_{bp}$  are found for  $n \geq 10$ .



**Figure S1:** The calculated  $MFR_{bp}$  for different numbers of bins,  $n$ .

## Description of Data from Figures

To facilitate comparison with other models and data sets the data from Figures 2-11 has been provided as individual text files. The specific data provided in each file for each figure is described in the tables below.

### Figure 2 (“Figure 2 Data.txt”)

The observations were taken from Faulhaber et al. (2009). The calculations were performed using the parameters given in Table S1. The data from the figure are included as a separate tab delimited file.

	Butanedioic Acid			Hexanedioic Acid			Decanedioic Acid		
	Cappa	C&Z	Average	Cappa	C&Z	Average	Cappa	C&Z	Average
$C_{sat}$ ( $\mu\text{g}/\text{m}^3$ )	1.5	6.5	3.1	0.14	1.78	0.5	0.0012	0.12	0.012
$\Delta H_{vap}$ (kJ/mol)	128	119.5	124	145.4	146	146	180	146.5	163

**Table S-1.** Thermodynamic parameters for the three dicarboxylic acids used to perform the calculations in Figure 2. “Cappa” = Cappa et al. (2007); C&Z = Chattopadhyay and Ziemann (2005).

Name	Description
T_But_Exp	$T_d$ ( $^{\circ}\text{C}$ ) for butanedioic acid from Faulhaber et al. (2009)
MFR_But_Exp	MFR for butanedioic acid from Faulhaber et al. (2009)
T_Hex_Exp	$T_d$ ( $^{\circ}\text{C}$ ) for hexanedioic acid from Faulhaber et al. (2009)
MFR_Hex_Exp	MFR for hexanedioic acid from Faulhaber et al. (2009)
T_Dec_Exp	$T_d$ ( $^{\circ}\text{C}$ ) for decanedioic acid from Faulhaber et al. (2009)
MFR_Dec_Exp	MFR for decanedioic acid from Faulhaber et al. (2009)
Td	Model $T_d$ ( $^{\circ}\text{C}$ )
MFR_But_Cappa	Model $\text{MFR}_{bp}$ for butanedioic acid using Cappa et al. thermo
MFR_But_Chat	Model $\text{MFR}_{bp}$ for butanedioic acid using C&Z thermo
MFR_But_Mean	Model $\text{MFR}_{bp}$ for butanedioic acid using Cappa and C&Z mean thermo
MFR_Hex_Cappa	Model $\text{MFR}_{bp}$ for hexanedioic acid using Cappa et al. thermo
MFR_Hex_Chat	Model $\text{MFR}_{bp}$ for hexanedioic acid using C&Z thermo
MFR_Hex_mean	Model $\text{MFR}_{bp}$ for hexanedioic acid using Cappa and C&Z mean thermo
MFR_Dec_Cappa	Model $\text{MFR}_{bp}$ for decanedioic acid using Cappa et al. thermo
MFR_Dec_Chat	Model $\text{MFR}_{bp}$ for decanedioic acid using C&Z thermo
MFR_Dec_mean	Model $\text{MFR}_{bp}$ for decanedioic acid using Cappa and C&Z mean thermo

**Figure 3** (“Figure 3 Data.txt”)

Name	Description
Td	Model $T_d$ (°C)
MFR_Profile	MFR <sub>bp</sub> using velocity profile
MFR_constant	MFR <sub>bp</sub> using constant velocity

**Figure 4** (“Figure 4 Data.txt”)

Name	Description
Csat	Saturation concentration, $C_{sat}$ ( $\mu\text{g}/\text{m}^3$ )
Dp	Particle diameter, $d_p$ (nm)
MFR_dp_low_loading	MFR <sub>bp</sub> as function of $d_p$ at $C_{OA} = 5 \mu\text{g}/\text{m}^3$
ResidenceTime	$t_{res}$ (s)
MFR_Csat	MFR <sub>bp</sub> as function of $C_{sat}$
MFR_dp_high_loading	MFR <sub>bp</sub> as function of $d_p$ at $C_{OA} = 150 \mu\text{g}/\text{m}^3$
MFR_Time	MFR <sub>bp</sub> as function of $t_{res}$

**Figure 5** (“Figure 5 Data.txt”)

Name	Description
Td	Model $T_d$ (°C)
MFR_10_Absorbent	MFR <sub>d</sub> at $C_{OA} = 10 \mu\text{g}/\text{m}^3$ for Case 1 (adsorbent denuder boundary condition)
MFR_10_NoLoss	MFR <sub>d</sub> at $C_{OA} = 10 \mu\text{g}/\text{m}^3$ for Case 3 (no loss boundary condition)
MFR_10_Eqm	MFR <sub>d</sub> at $C_{OA} = 10 \mu\text{g}/\text{m}^3$ for Case 2 (local equilibrium boundary condition)
MFR_100_Absorbent	MFR <sub>d</sub> at $C_{OA} = 100 \mu\text{g}/\text{m}^3$ for Case 1 (adsorbent denuder boundary condition)
MFR_100_NoLoss	MFR <sub>d</sub> at $C_{OA} = 100 \mu\text{g}/\text{m}^3$ for Case 3 (no loss boundary condition)
MFR_100_Eqm	MFR <sub>d</sub> at $C_{OA} = 100 \mu\text{g}/\text{m}^3$ for Case 2 (local equilibrium boundary condition)
MFR_500_Absorbent	MFR <sub>d</sub> at $C_{OA} = 500 \mu\text{g}/\text{m}^3$ for Case 1 (adsorbent denuder boundary condition)
MFR_500_NoLoss	MFR <sub>d</sub> at $C_{OA} = 500 \mu\text{g}/\text{m}^3$ for Case 3 (no loss boundary condition)
MFR_500_Eqm	MFR <sub>d</sub> at $C_{OA} = 500 \mu\text{g}/\text{m}^3$ for Case 2 (local equilibrium boundary condition)

**Figure 6** (“Figure 6x Data.txt”)

The data in each file (e.g. “Figure 6x Data.txt”) comes from the corresponding panel x (e.g. x = a, b, c, etc.). “Distance” is the distance from the thermodenuder entrance (in cm). The other columns “Radius\_X\_Y” (where X indicates the loading condition, either “high” or “low,” and Y indicates boundary condition case) are in order from closest to the TD center to closest to the TD walls.

**Figure 7** (“Figure 7 Data.txt”)

Name	Description
Td	Model $T_d$ (°C)
MFR_15sec_10ug	MFR <sub>h</sub> at $t_{res} = 15$ seconds and $C_{OA} = 10 \mu\text{g}/\text{m}^3$
MFR_30sec_10ug	MFR <sub>h</sub> at $t_{res} = 30$ seconds and $C_{OA} = 10 \mu\text{g}/\text{m}^3$
MFR_60sec_10ug	MFR <sub>h</sub> at $t_{res} = 60$ seconds and $C_{OA} = 10 \mu\text{g}/\text{m}^3$
MFR_15sec_100ug	MFR <sub>h</sub> at $t_{res} = 15$ seconds and $C_{OA} = 100 \mu\text{g}/\text{m}^3$
MFR_30sec_100ug	MFR <sub>h</sub> at $t_{res} = 30$ seconds and $C_{OA} = 100 \mu\text{g}/\text{m}^3$
MFR_60sec_100ug	MFR <sub>h</sub> at $t_{res} = 60$ seconds and $C_{OA} = 100 \mu\text{g}/\text{m}^3$
MFR_15sec_500ug	MFR <sub>h</sub> at $t_{res} = 15$ seconds and $C_{OA} = 500 \mu\text{g}/\text{m}^3$
MFR_30sec_500ug	MFR <sub>h</sub> at $t_{res} = 30$ seconds and $C_{OA} = 500 \mu\text{g}/\text{m}^3$
MFR_60sec_500ug	MFR <sub>h</sub> at $t_{res} = 60$ seconds and $C_{OA} = 500 \mu\text{g}/\text{m}^3$

**Figure 8** (“Figure 8x Data.txt”), where x corresponds to the panel a, b, c or d

*Figure 8a*

Name	Description
Td	Model $T_d$ (°C)
MFR_1000	MFR <sub>bp</sub> for $C_{sat} = 1000 \mu\text{g}/\text{m}^3$
MFR_100	MFR <sub>bp</sub> for $C_{sat} = 100 \mu\text{g}/\text{m}^3$
MFR_10	MFR <sub>bp</sub> for $C_{sat} = 10 \mu\text{g}/\text{m}^3$
MFR_1	MFR <sub>bp</sub> for $C_{sat} = 1 \mu\text{g}/\text{m}^3$
MFR_01	MFR <sub>bp</sub> for $C_{sat} = 0.1 \mu\text{g}/\text{m}^3$
MFR_001	MFR <sub>bp</sub> for $C_{sat} = 0.01 \mu\text{g}/\text{m}^3$
MFR_0001	MFR <sub>bp</sub> for $C_{sat} = 0.001 \mu\text{g}/\text{m}^3$

*Figure 8b*

Name	Description
Td	Model $T_d$ (°C)
MFR_40kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 40 \text{ kJ/mol}$
MFR_60kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 60 \text{ kJ/mol}$
MFR_80kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 80 \text{ kJ/mol}$
MFR_100kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 100 \text{ kJ/mol}$
MFR_120kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 120 \text{ kJ/mol}$
MFR_140kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 140 \text{ kJ/mol}$
MFR_160kJ	MFR <sub>bp</sub> for $\Delta H_{vap} = 160 \text{ kJ/mol}$

Figure 8c

Name	Description
Csat	Saturation concentration ( $\mu\text{g}/\text{m}^3$ )
T50inv_120kJ_300nm	$1/T_{50}$ (in 1/K) for $\Delta H_{\text{vap}} = 120$ kJ/mol and $d_p = 300$ nm
T50inv_150kJ_200nm	$1/T_{50}$ (in 1/K) for $\Delta H_{\text{vap}} = 150$ kJ/mol and $d_p = 200$ nm
T50inv_faulhaber	$1/T_{50}$ (in 1/K) from Faulhaber et al. (2009)

Figure 8d

Name	Description
DH	Enthalpy of vaporization, $\Delta H_{\text{vap}}$ (kJ/mol)
T50_DH	$T_{50}$ ( $^{\circ}\text{C}$ )

Figure 9 (“Figure 9 Data.txt”)

Name	Description
dp	Particle diameter, $d_p$ (nm)
T50_5_5	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 5$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 5$ $\mu\text{g}/\text{m}^3$
T50_50_5	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 5$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 50$ $\mu\text{g}/\text{m}^3$
T50_150_5	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 5$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 150$ $\mu\text{g}/\text{m}^3$
T50_250_5	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 5$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 250$ $\mu\text{g}/\text{m}^3$
T50_5_01	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 0.1$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 5$ $\mu\text{g}/\text{m}^3$
T50_50_01	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 0.1$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 50$ $\mu\text{g}/\text{m}^3$
T50_150_01	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 0.1$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 150$ $\mu\text{g}/\text{m}^3$
T50_250_01	$T_{50}$ ( $^{\circ}\text{C}$ ) for $C_{\text{sat}} = 0.1$ $\mu\text{g}/\text{m}^3$ and $C_{OA} = 250$ $\mu\text{g}/\text{m}^3$

Figure 10 (“Figure 10 Data.txt”)

Name	Description
Di	Diffusion coefficient, $D_i$ ( $\text{m}^2/\text{s}$ )
T50_300_5	$T_{50}$ for $d_p = 300$ nm and $C_{OA} = 5$ $\mu\text{g}/\text{m}^3$
T50_300_250	$T_{50}$ for $d_p = 300$ nm and $C_{OA} = 250$ $\mu\text{g}/\text{m}^3$
T50_100_5	$T_{50}$ for $d_p = 100$ nm and $C_{OA} = 5$ $\mu\text{g}/\text{m}^3$

**Figure 11**

TarrayForTD	Model $T_d$ (°C)
MFR_f0	MFR <sub>bp</sub> for a non-volatile core that is 0% of the total particle mass (panel a)
MFR_f01	MFR <sub>bp</sub> for a non-volatile core that is 10% of the total particle mass (panel a)
MFR_f02	MFR <sub>bp</sub> for a non-volatile core that is 20% of the total particle mass (panel a)
MFR_f03	MFR <sub>bp</sub> for a non-volatile core that is 30% of the total particle mass (panel a)
MFR_f04	MFR <sub>bp</sub> for a non-volatile core that is 40% of the total particle mass (panel a)
MFR_f05	MFR <sub>bp</sub> for a non-volatile core that is 50% of the total particle mass (panel a)
MFRnv_f05	MFR <sub>bp</sub> for a non-volatile absorptive component that is 50% of the total particle mass (panel b)
MFRnv_f04	MFR <sub>bp</sub> for a non-volatile absorptive component that is 40% of the total particle mass (panel b)
MFRnv_f03	MFR <sub>bp</sub> for a non-volatile absorptive component that is 30% of the total particle mass (panel b)
MFRnv_f02	MFR <sub>bp</sub> for a non-volatile absorptive component that is 20% of the total particle mass (panel b)
MFRnv_f01	MFR <sub>bp</sub> for a non-volatile absorptive component that is 10% of the total particle mass (panel b)

**Figure 12**

“Figure 12 Data-1.txt”

Name	Description
Td	Model $T_d$ (°C)
MFRbp	MFR <sub>bp</sub> for total OA
MFRh	MFR <sub>h</sub> for total OA
MFRd	MFR <sub>d</sub> for total OA

“Figure 12 Data-2.txt”

Name	Description
Td	Model $T_d$ (°C)
MFRbp_compounds	MFR <sub>bp</sub> for individual compounds, in order from highest $C_{sat}$ (100 $\mu\text{g}/\text{m}^3$ ) to lowest $C_{sat}$ ( $10^{-3}$ $\mu\text{g}/\text{m}^3$ )

## References

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